

**TRANSMITTAL LETTER TO THE UNITED STATES
DESIGNATED/ELECTED OFFICE (DO/EO/US)
CONCERNING A FILING UNDER 35 U.S.C. 371**

U.S. APPLICATION NO. (IF KNOWN, SEE 37 CFR)

09/889875INTERNATIONAL APPLICATION NO.
PCT/US00/04105INTERNATIONAL FILING DATE
18 FEBRUARY 2000 (18.02.00)PRIORITY DATE CLAIMED
19 FEBRUARY 1999 (19.02.99)

TITLE OF INVENTION

TOUGHENED, HIGH-MODULUS POLYAMIDES

APPLICANT(S) FOR DO/EO/US

WEINBERG, Mark

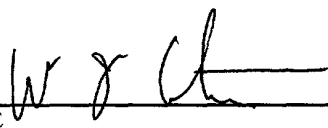
Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information

1. ☒ This is a **FIRST** submission of items concerning a filing under 35 U.S.C. 371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. 371.
3. ☒ This is an express request to being national examination procedures (35 U.S.C. 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. 371(b)) and PCT Articles 22 and 39(1).
4. ☒ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5. ☒ A copy of the International Application was filed (35 U.S.C. 371 (c) (2))
 - a. ☒ is transmitted herewith (required only if not transmitted by the International Bureau.
 - b. ☐ has been transmitted by the International Bureau.
 - c. ☐ is not required, as the application was filed in the United States Receiving Office (RO/US)
6. ☐ A translation of the International Application into English (35 U.S.C. 371 (c) (2)).
7. ☒ A copy of the International Search Report (PCT/ISA/210).
8. ☒ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371 (c) (3))
 - a. ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☐ have been transmitted by the International Bureau.
 - c. ☐ have not been made; however, the time limit for making such amendments has NOT expired.
 - d. ☒ have not been made and will not be made.
9. ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371 (c)(3)).
10. ☒ An oath or declaration of the inventor(s) (35 U.S.C. 371 (c)(4)).
11. ☒ A copy of the International Preliminary Examination Report (PCT/IPEA/409)
12. ☐ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371 (c)(5)).

Items 13 to 18 below concern document(s) or information included :

13. ☐ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
14. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
15. ☐ A **FIRST** preliminary amendment.
A **SECOND** or **SUBSEQUENT** preliminary amendment.
16. ☐ A substitute specification.
17. ☒ A change of power of attorney and/or address letter.
18. ☒ Certificate of Mailing by Express Mail.
19. ☐ Other items or information:

17. General Power of Attorney**18. Express Mailing Label No.: EL031053808US**

APPLICATION NO. (UNKNOWN, 37 CFR) 09/889875		INTERNATIONAL APPLICATION NO. PCT/US00/04105		ATTORNEY'S DOCKET NUMBER CL-1375	
29. The following fees are submitted* BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5)) : <input checked="" type="checkbox"/> Search Report has been prepared by the EPO or JPO \$860.00 <input type="checkbox"/> International preliminary examination fee paid to USPTO (37 CFR 1.482) \$690.00 <input type="checkbox"/> No international preliminary examination fee paid to USPTO (37 CFR 1.482) but international search fee paid to USPTO (37 CFR 1.445(a)(2)) \$760.00 <input type="checkbox"/> Neither international preliminary examination fee paid to USPTO (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO \$1000.00 <input type="checkbox"/> International preliminary examination fee paid to USPTO (37 CFR 1.482) And all claims satisfied provisions of PCT Article 33(2)-(4) \$ 100.00					CALCULATIONS PTO USE ONLY
ENTER APPROPRIATE BASIC FEE AMOUNT =					\$860.00
Surcharge of \$130.00 for furnishing the oath or declaration later than months from the earliest claimed priority date (37 CFR 1.492 (e)). <input type="checkbox"/> 20 <input type="checkbox"/> 30					\$0.00
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE		
Total Claims	17 - 20 =	0 x	\$18.00	\$0.00	
Independent Claims	2 - 3 =	0 x	\$80.00	\$0.00	
Multiple Dependent Claims (check if applicable)			<input type="checkbox"/>	\$0.00	
TOTAL OF ABOVE CALCULATIONS =				\$0.00	
Reduction of 1/2 for filing by small entity, if applicable. Verified Small Entity Statement must also be filed (Note 37 CFR 1.9, 1.27, 1.28) (check if applicable). <input type="checkbox"/>				\$0.00	
SUBTOTAL =				\$0.00	
Processing Fee of \$130.00 for furnishing the English translation later than months from the earliest claimed priority date (37 CFR 1.492 (f)). <input type="checkbox"/> 20 <input type="checkbox"/> 30				\$0.00	
TOTAL NATIONAL FEE =				\$860.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31) (check if applicable). <input type="checkbox"/>				\$0.00	
TOTAL FEES ENCLOSED =				\$860.00	
				Amount to be : refunded	\$
				Charged	\$
<input type="checkbox"/> A check in the amount of _____ to cover the above fees enclosed. <input checked="" type="checkbox"/> Please charge my Deposit Account No. 04-1928 in the amount of \$860.00 to cover the above fees. <input checked="" type="checkbox"/> The Commissioner is hereby authorized to charge any fees which may be required, or credit any overpayment to Deposit Account No. 04-1928 a duplicate copy of this sheet is enclosed.					
NOTE : Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (CFR 1.37(a) or (b)) must be filed and granted to restore the application to pending status.					
SEND ALL CORRESPONDENCE TO:					
COTREAU, William Joseph E. I. DU PONT DE NEMOURS AND COMPANY Legal Patent Records Center 1007 Market Street Wilmington, Delaware 19898 United States of America			SIGNATURE  COTREAU, WILLIAM JOSEPH NAME 36,490 REGISTRATION NUMBER 16 July 2001 DATE		

Referring to data in Table 1, a Zytel® 408L plasticized nylon resin exhibits a 330% improvement in impact strength but at about 230% reduction in stiffness in comparison to the general purpose Zytel® 101 resin. Plasticizers in general improve processibility, but degrade numerous other mechanical properties. Elastomer filled Zytel® ST801 known as a “rubber toughened” or “super-tough” nylon composition exhibits about a 1600% improvement in toughness, but at

about a 40% loss in stiffness in comparison to the general purpose Zytel® 101 resin. Additionally, rubber toughened nylons are expensive to produce.

With continuing reference to Table 1, blending short glass fibers in a nylon resin composition (e.g., Zytel® 71G33L) provides about 140% improvement in toughness and about a 140% increase in stiffness over the Zytel® 101. However, glass fibers significantly reduce the moldability of the resulting resin and may lead to property anisotropy, uneven shrinkage, and part warpage. Mineral fillers provide similar improvements in stiffness to the nylon resin but at about a 40% reduction in toughness, even though processibility and product isotropy are improved.

U.S. Patent No. 4,399,246, to Hyde discloses polyamide compositions comprising 50 to 75 parts of resin, 25 to 50 parts of mineral filler, 0.2 to 0.9 parts of aminofunctional silane, and 0.2 to 0.9 parts of a sulfonamide. The mineral fillers include calcined clay, wollastonite, and talc in the size range of 0.2 to 2 micrometers. The stiffness of filled nylon 66 was 5865 MPa while Izod impact resistance was about 65 J/m.

U.S. Patent No. 4,740,538, to Sekutowski discloses a nylon composition containing a kaolin filler precoated with an amino functional silane, the composition further containing a phenol or triethanolamine as an impact modifier.

Wu et al, Proc. Inter. Conf. Pet. Ref. and Petrochem. Proc., 2, pp 802ff (1991) discloses employing a rubber coated CaCO₃ to effect improvements in impact resistance of nylon 6.

U.S. Patent No. 5,571,851 to Freeman et al. discloses an Izod impact of 42.6 J/m (0.76 ft-lbs/in) and a flexural modulus of 5620 MPa (816 ksi) when a combination of 25% stearylsilane and 75% aminosilane is incorporated into a composition of nylon 66 and calcined clay comprising 40% of calcined clay. When only the stearylsilane is employed both flexural modulus and Izod impact resistance are significantly lower.

It is known in the art to incorporate fatty acids, particularly stearic acid, into mineral filled polyolefin compositions. For example, U.S. Patent No. 4,795,768 to Ancker et al. discloses a composition consisting of high density polyethylene filled with 50 wt-% of a 3.5 µm CaCO₃ pre-treated with 2% by weight of isostearic acid. Izod impact was decreased by about 68% with respect to the unfilled polymer while flexural modulus was increased by about 150%.

Orange, 10th Int. Conf. Deformation, Yield, and Fracture of Polymers, Inst. of Mat., pp. 502ff, (1997) discloses filled polypropylene compositions containing 10% by volume of a 0.1 µm and 2 µm CaCO₃ both stearic acid treated and untreated. The compositions containing the stearic acid treated fillers

exhibited fracture toughness higher than the unfilled polymer and somewhat higher stiffness. The composition containing the 2 μm untreated filler was similar to the treated composition, but that containing the 0.1 μm untreated filler exhibited a 50% reduction in fracture toughness and about a 45% increase in stiffness.

Suetsugu, The Polymer Processing Society, 6, (1990), discloses an increase of notched Izod impact resistance of 230% in a high molecular weight polypropylene composition containing 30% by weight of stearic acid treated 4.3 μm CaCO_3 .

U.S. Patent No. 3,926,873 to Aishima et al. discloses compositions comprising inorganic fillers, unsaturated carboxylic acids, and nylon 6 and nylon 66 polymers. Improvements in Izod impact resistance of less than 50% are realized while flexural modulus is increased by 50%. The process of Aishima requires a preliminary reaction step between the filler and the unsaturated carboxylic acid, followed by melt processing with the polymer in the presence of a free-radical generator.

The differences between saturated and unsaturated fatty acids in their interaction with mineral particles is disclosed in Ottewill et al., J. Oil Colour Chemists Assn, 50:844 (1967).

SUMMARY OF THE INVENTION

In one aspect of the present invention, there is provided a composition comprising nylon 6, nylon 66, or a mixture thereof, about 1%-50% by volume of a mineral filler having an aspect ratio of less than about 5, the filler having an average equivalent spherical diameter in the range of about 0.1 to less than about 3.5 micrometers, and a saturated organic acid, salt thereof, or a mixture thereof, at a concentration of at least about 0.5% by weight of the mineral filler.

In another aspect, the invention relates to a process for forming a composition, comprising the steps of: combining nylon 6, nylon 66, or a mixture thereof with a mineral filler having an aspect ratio of less than 5, the mineral filler having an average equivalent spherical diameter in the range of about 0.1 to about 3.5 micrometers, and a saturated organic acid, salt thereof, or a mixture thereof, at a concentration of at least about 0.5% by weight of the mineral filler, the mineral filler and the nylon being combined at a weight ratio given by the formula:

$$W_f/W_p = [VF/(1-VF)] \cdot D_f/D_p$$

where W_f is the weight of the filler, W_p is the weight of the polymer, VF is the desired volume fraction of filler, in the range of about 0.01-0.5, D_f is the density of the filler, and D_p is the density of the polymer;

heating the combination to a temperature above the melting point of the nylon to form a molten composition;

mixing the molten composition to provide a homogenous melt; and, cooling the molten composition.

5

DETAILED DESCRIPTION

This invention, through the incorporation of saturated organic acids, salts thereof, or mixtures thereof, into compositions comprising polyamides and mineral fillers, results in improvements in properties over the unfilled polymer and filled polymers containing impact modifiers of the art. This invention improves stiffness at constant toughness, toughness at constant stiffness, and, in certain embodiments, simultaneously improves stiffness and toughness.

Nylon 6, nylon 66, and mixtures thereof, including nylon resins which have been nucleated, pigmented, and otherwise modified, are suitable for the practice of this invention. The nylons of this invention may include small amounts of common additives, typically less than 5% by weight, which may affect toughness or stiffness, including: glass fibers, carbon black, plasticizers, pigments, and other well-known additives commonly employed in the art.

Suitable inorganic fillers for use in this invention are those that do not have significant off-gassing or decompose at typical polyamide processing conditions. These include, but are not limited to: calcium carbonate; oxides such as alumina, silica, and titanium dioxide; sulfates such as barium sulfate; titanates; kaolin clay and other silicates; magnesium hydroxide, and carbon black. In the present invention, an aspect ratio (the average ratio of the largest to the smallest dimension of the filler particle) of less than about 5 avoids stress concentrations and part anisotropies. The preferred fillers are calcium carbonate and titanium dioxide.

The size of the filler particles is stated as the equivalent spherical diameter. The equivalent spherical diameter is the diameter of a sphere having the same volume as the filler particle and may be determined by use of a Sedigraph 5100 (Micrometrics Instrument Corporation, Norcross, GA). The Sedigraph 5100 determines particle size by the sedimentation method, measuring the gravity-induced settling rates of different size particles in a liquid with known properties. The rate at which particles fall through the liquid is described by Stokes' Law. The largest particles fall fastest, while the smallest particles fall slowest. The sedimentation rate is measured using a finely collimated beam of low energy X-rays which pass through the sample cell to a detector. The distribution of particle mass at various points in the cell affects the number of X-ray pulses reaching the detector. This X-ray pulse count is used to derive the particle size

The size of the filler particles can affect the toughness and/or stiffness properties of the composition of the invention. Particles that are either too large or too small do not produce the benefits of the present invention. A suitable filler particle has a relatively narrow size distribution with particular emphasis on having a minimum number of particles much larger than the mean particle size.

The relationship among mean nearest neighbor interparticle distance (IPD), filler size, d , and required filler loading, ϕ (as a volume fraction), is given approximately by the equation

$$25 \quad \text{IPD} = d \cdot [(\pi/6\phi)^{1/3} - 1].$$

5

conditions are no longer favorable for debonding, making these particles sizes unsuitable.

It is believed that the polymer/filler interfacial forces are mediated by one or more saturated organic acids or salts thereof. The requisite amount depends upon the interfacial area -- e.g., the greater the interfacial area, the more organic acid or acid salt is required. The actual amount however will depend upon the size and shape of the particles and the volume loading of the particles.

It is found that the concentration of filler varies with filler size, increasing with increasing size in the suitable range. Thus, if the filler size is at the high end of the range, a higher concentration of filler is needed than if the filler size is at the lower end of the range. The suitable range is about 1 to about 50 vol. %, preferably about 5 to about 30 vol %, and most preferably about 10 to about 20 vol %. One of skill in the art, will recognize, however, that at 1% filler loadings, nylon compositions will exhibit minimal improvements in stiffness or impact resistance.

At filler loadings greater than approximately 30 vol %, it becomes increasingly difficult to achieve a homogeneous distribution of non-agglomerated filler within the polymer matrix using ordinary methods of melt mixing. Hence, filler concentrations of 30-50 vol % are a less preferred embodiment of the present invention.

Suitable saturated organic acids include aliphatic carboxylic acids having about 6-30 carbon atoms optionally substituted by one or more oxygen atoms or sulfur atoms. A suitable acid may optionally contain one or more aliphatic, aromatic, or functionalized side chains. Preferred organic acids include stearic acid. Inorganic salts of the suitable acids are equally suitable, including zinc stearate and the like. It is understood by one of skill in the art that an organic acid in combination with a mineral at elevated temperatures may form a salt therewith so that the acid added to the mixture in the process of the invention may or may not be present in the final product thereof. The organic acids or salts thereof are present at a concentration of at least 0.5% by weight on the weight of the filler. While there is no particular upper limit to concentration of organic acid, in one embodiment of the invention the concentration of organic acid or salt thereof is in the range of about 0.5-to about 4% by weight on the weight of the filler.

It is believed that a useful concentration of acid or acid salt in the composition of the invention corresponds to that at which the acid or salt forms a molecular monolayer on substantially all of the mineral filler surface. Any amount less than that will exhibit less than the optimal combination of properties while any amount more than that serves no function except to dilute the amount of

polymer in the composition. The addition of about 2% by weight of stearic acid on the weight of the 0.7 μm CaCO_3 is optimal.

The composition of the invention is formed by coating a filler with a saturated organic acid or salt thereof, mixing the coated filler into the polyamide, and pelletizing the product. The saturated organic acids or salts may be, but are not required to be, applied to the filler in a separate coating step prior to processing with polymer. In a method, known in the art, for applying organic acid or salt coatings to mineral fillers, the acid or salt is dissolved in an appropriate solvent and mixed with the filler until it is all coated. The thus coated filler can then be separated from the solution and the remaining solvent removed by drying. In another method, the acid or acid salt, the filler and the polymer are combined at once. Mixing may further be achieved by dispersing the filler into a dispersion or solution of the polymer and the organic acid or salt thereof, followed by drying; Mixing may also be achieved in the melt, either in a batch mixer or a continuous extruder.

Preferably, the ingredients are dry-blended by tumbling followed by feeding to an extruder or batch mixer according to well-established methods of the art. Alternatively, the ingredients can be separately and continuously fed to one or more extruder zones by, for example, the use of weight loss feeders, all of the mixing being performed in the extruder; or the material may be added at once or in stages to a batch type melt blender and the composition formed therein.

In one embodiment of the invention, the ingredients are processed in a twin-screw co-rotating extruder to ensure good mixing. The extrudate is pelletized and subsequently molded into parts by injection molding. The pellets can also be compression molded or a molded or extruded sheet can be thermoformed into a complex shape. Other means known in the art may also be employed to form shaped articles of the composition of the invention.

It is convenient to combine the nylon polymer and filler according to a weight ratio determined by the respective densities thereof and the goal volume fraction of filler. The weight ratio is determined from the equation

$$W_f/W_p = [VF/(1-VF)] \cdot D_f/D_p$$

where W_f is the weight of the filler, W_p is the weight of the polymer, VF is the desired volume fraction of filler, in the range of about 0.01-0.5 as herein described, D_f is the density of the filler, and D_p is the density of the polymer. The density, D , is not the bulk density but the actual density of the material.

The present invention is further illustrated by the following specific embodiments which are not intended to be limiting thereon.

EXAMPLES

In the following examples, all fillers and resins were dried at 90°C overnight prior to dry-mixing. Melt blending was accomplished in a 28 mm co-rotating twin screw extruder (Werner & Pfleiderer, Ramsey, NJ) at the temperatures and concentrations hereinbelow specified. The extrudate was pelletized. The extruded pellets were dried overnight at 90°C and then processed in a 6 oz., 150 ton Van Dorn injection molding machine equipped with a water-heated mold, into dog-bone shaped tensile bars for tensile testing according to ASTM D638-95 (Type I specimen, 2" long gauge length; 1/2" wide; 1/8" thick) and flexural test bars (5" long, 1/2" wide, 1/8" thick).

The injection molded flexural test bars were then divided into two 2-1/2" long pieces, one close to the gate and referred to as the "near end" and the other far from the gate and referred to as the "far end". Notches of root radius 0.01" were cut into each part with a TMI Notching Cutter according to the process described in ASTM D256. The impact response was studied in notched Izod impact tests according to ASTM D256. Flexural testing was performed according to ASTM D790, with a cross head rate of 0.127 cm/min (0.05 inch/min). The values of the mechanical parameters determined from flexural and Izod tests were calculated as averages over measurements on at least 3 specimens. The standard deviation for Izod results was about 0.53 J/m (0.01 ft-lb/in).

In Examples 1-5, and Comparative Examples 1-17, the compounding extruder barrel temperature was 240°C, and the throughput rate was about 9.1 kg/hr (20 lbs/hour). Injection molding was conducted with a barrel temperature of 240°C and a mold temperature of 40°C.

EXAMPLES 1-2 AND COMPARATIVE EXAMPLES 1-7

Capron 8202 nylon 6 (Allied-Signal, Richmond, VA) was injection molded without filler in Comparative Example (Comp. Ex.) 1.

In Comparative Examples 2 and 3, Ti-Pure® R101, uncoated 0.29 µm titanium dioxide (DuPont Company, Wilmington, DE) was melt blended with Capron 8202 at concentrations of 5 and 10 vol %, respectively.

In Examples (Ex.) 1 and 2, 50 grams of stearic acid (SA) was mixed with 150 grams of chloroform in a beaker. 5000 grams of uncoated Ti-Pure® R-104-DD TiO₂ was charged into a powder mixer. The solution was added with a pipet while the TiO₂ (titanium dioxide) was stirred. After the addition was complete, the mixture was stirred for 3 minutes at medium speed and then dried at 100°C for 2 hours.

The stearic acid (SA) treated titanium dioxide so produced was melt blended with Capron 8202 at concentrations of 5 and 10 vol % respectively, and molded into test bars.

- 5 In Comparative Examples 4 and 5, Ti-Pure[®] R104 0.22 μ m titanium dioxide coated with octa-triethoxy silane (OTES) was obtained from DuPont, melt blended with Capron 8202 at concentrations of 5 and 10 vol %, respectively, and molded into test bars.

- 10 In Comparative Examples 6 and 7, 3000 grams of uncoated Ti-Pure[®] R-104-DD TiO₂ was charged into a powder mixer. Thirty grams of 3-aminopropyl triethoxy silane was added by dropping pipet while the TiO₂ was stirred. After the addition was complete, the mixture was stirred for 3 minutes at medium speed. The product was then dried at 100°C for 2 hours.

The APS treated titanium dioxide was melt blended with Capron 8202 at concentrations of 5 and 10 vol %, respectively, and molded into test bars.

- 15 The test results in Table 2 show that the stearic acid coated particles have a surprising increase in Izod toughness as the filler volume is increased, whereas, the other examples show a decrease in Izod toughness.

Table 2							
Properties of TiO ₂ -filled Nylon 6							
Example	Surface Treatment	Vo. % TiO ₂	Izod (ft-lb/in)		Izod (J/m)		
			Near End	Far End	Near End	Far End	
Comp. Ex. 1	N.A.	0	1.1	1.1	58.3	58.3	
Ex. 1	SA	5	1.3	1.3	68.9	68.9	
Ex. 2	SA	10	1.3	1.5	68.9	79.5	
Comp. Ex. 2	Uncoated	5	0.9	0.98	47.7	51.94	
Comp. Ex. 3	Uncoated	10	0.9	0.84	47.7	44.52	
Comp. Ex. 4	OTES	5	1.1	1.2	58.3	63.6	
Comp. Ex. 5	OTES	10	0.98	1.1	51.94	58.3	
Comp. Ex. 6	APS	5	1.1	1.2	58.3	63.6	
Comp. Ex. 7	APS	10	0.87	1.1	46.11	58.3	

EXAMPLES 3-5 AND COMPARATIVE EXAMPLES 8-17

For Comparative Example 8, Capron 8200 nylon 6 was injection molded without filler. In Comparative Examples 9-11, Albafil (AF) uncoated 0.7 μm calcium carbonate (Specialty Minerals Inc., Bethlehem, PA) was melt blended with Capron 8200 nylon 6 (Allied-Signal, Somerville NJ) at concentrations of 5, 10, and 20 vol % respectively, and injection molded into test bars.

In Comparative Examples 12-14, 1500 grams of uncoated 0.7 μm Albafil was dried at 150°C in a vacuum oven overnight. This material was then placed into a resin kettle with 2 liters of ethanol. A separate solution of 100 grams of Zonyl-UR, a fluorosurfactant available from DuPont, in 1 liter of ethanol was heated to 80°C for 0.5 hour. The two mixtures were combined and stirred for 5 hours. The slurry so formed was allowed to settle for 3 days and then filtered with a Buchner funnel and dried overnight in an 80°C vacuum oven.

In Comparative Examples 15-17, 1500 grams of undried, uncoated 0.7 μm Albafil was mixed with 1500 ml of hexane. A separate solution of 20 grams of APS in 500 ml of hexane was added to the Albafil dispersion and the mixture stirred for 5 hours, filtered by Buchner funnel, and dried overnight in a 100°C vacuum oven.

In Examples 3-5, Super-Pflex 200 (S200 or SPF) stearic acid-coated 0.7 micrometer calcium carbonate was obtained from Specialty Minerals, Inc. The three thus-treated calcium carbonate compositions were melt blended with Capron 8200 nylon 6 at concentrations of each of 5 vol %, 10 vol %, and 20 vol %, and all subsequently molded into test bars and the test results are provided in Table 3. The results shown in Table 3 demonstrate that S200 with a fatty acid surface coating causes a increase in izod toughness. None of the other surface treatments on the identical CaCO_3 , shown in Table 3, result in the same phenomenon.

<p>Table 3</p> <p>Properties of CaCO₃-filled nylon 6</p>									
Example	FILLER	Surface Treatment	Vol. % CaCO ₃	Izod (ft-lb/in)		Izod (J/m)			
Comp. Ex. 8	NONE		0	Near End	Far End	Near End	Far End		
Comp. Ex. 9	Albafil	None	5	0.6	0.7	31.8	37.1		
Comp. Ex. 10	Albafil	None	10	0.6	0.62	31.8	32.86		
Comp. Ex. 11	Albafil	None	20	0.76	0.81	40.28	42.93		
Ex. 3	S200	SA	5	1.57	1.79	83.21	94.87		
Ex. 4	S200	SA	10	1.81	2.27	95.93	120.31		
Ex. 5	S200	SA	20	2.08	2.3	110.24	121.9		
Comp. Ex. 12	Albafil	Zonyl-UR	5	0.76	0.92	40.28	48.76		
Comp. Ex. 13	Albafil	Zonyl-UR	10	0.92	1	48.76	53		
Comp. Ex. 14	Albafil	Zonyl-UR	20	0.65	0.57	34.45	30.21		
Comp. Ex. 15	Albafil	APS	5	0.76	0.81	40.28	42.93		
Comp. Ex. 16	Albafil	APS	10	0.81	0.81	42.93	42.93		
Comp. Ex. 17	Albafil	APS	20	0.81	0.87	42.93	46.11		

EXAMPLES 6-10 AND COMPARATIVE EXAMPLES 18-24

- In Comparative Example 18, high viscosity Zytel® 42A nylon 66 (DuPont) was injection molded without filler. The three calcium carbonate fillers of different average particle sizes, listed in Table 4 were obtained from Specialty Minerals Inc. All three fillers were similarly surface treated with stearic acid. Each of the three were melt blended and molded into test bars at the concentrations shown with Zytel® 42A nylon 66 with the extruder and molding machine barrel temperatures at 270°C and the mold temperature at 90°C. The results of Izod testing of these samples are shown in Table 4. The data of Table 4 shows that both stiffness and impact resistance are simultaneously enhanced with filler particles within a range of about 0.1 to less than about 3.5 microns.. Table 4 shows that at filler sizes below this range, of 0.07 μm , and at 3.5 μm the Izod values did not increase.

Table 4													
Properties of Stearic Acid Treated CaCO ₃ -filled Nylon 66													
Example	Filler	Filler Size (μm)	Vol. % CaCO ₃	Izod (ft-lb/in)		Izod (J/μ)		Flex Mod. (ksi)	Flex Mod MPa	Flex Strength (ksi)	Flex Strength MPa	Elong. %	
				Near End	Far End	Near End	Far End						
Comp. Ex. 18	None	-	0	1.04	1.1	55.12	58.3	414	2860	15.97	110	97.5	
Ex. 6	S200	0.7	5	0.8	0.88	42.4	46.64	448	3090	16.73	120	66.7	
Ex. 7	S200	0.7	10	0.8	1.07	42.4	56.71	472	3260	15.41	110	33.3	
Ex. 8	S200	0.7	15	1.28	1.74	67.84	92.22	506	3490	14.76	100	48.3	
Ex. 9	S200	0.7	20	1.58	2	83.74	106	541	3730	13.83	100	48.3	
Ex. 10	S200	0.7	25	1.6	1.71	84.8	90.63	573	3950	12.69	90	54.2	
Comp. Ex. 19	UPF*	0.07	5	0.75	0.8	39.75	42.4						
Comp. Ex. 20	UPF*	0.07	15	0.56	0.56	29.68	29.68						
Comp. Ex. 21	UDF*	0.07	25	0.4	0.4	21.2	21.2						
Comp. Ex. 22	HPF**	3.5	5	0.8	0.8	42.4	42.4						
Comp. Ex. 23	HPF**	3.5	25	0.8	0.8	42.4	42.4						
Comp. Ex. 24	HPF**	3.5	30	0.72	0.78	38.16	41.34						

- In Comparative Example 25, general purpose viscosity Zytel® 101 nylon 66 (DuPont) was injection molded without filler. In Examples 11-14, Super-Pflex® 200 calcium carbonate was melt blended with Zytel® 101 and the resulting composition molded into test bars similar to Examples 6-10 in Table 4 except that the mold temperature was lowered to 40°C.

Table 5					
Properties of 0.7 μm CaCO ₃ -filled nylon 66					
Example	Vol % Super-Pflex. 200	Izod (ft-lb/in)		Izod(J/m)	
		Near End	Far End	Near End	Far End
Comp. Control Ex. 25	0	1.3	1.2	68.9	63.6
Ex. 11	5	1	1.1	53	58.3
Ex. 12	10	0.9	1	47.7	53
Ex. 13	20	1.5	1.9	79.5	100.7
Ex. 14	25	1.1	1.4	58.3	74.2

EXAMPLES 15-19 AND COMPARATIVE EXAMPLES 26-32

- The conditions of Examples 6-10 and Comparative Examples 18-24 described above were repeated for Examples 15-19 and Comparative Examples 26-32 with the exception that the polymer was Zytel® 132F, a nylon 66 resin (DuPont), and the concentrations were as shown in Table 6. The results with S200 show an increase in Izod toughness with increasing volume % at a filler size of .7 μm . Negligible increase in Izod toughness was obtained with fillers of 0.07, below the range of 0.1 to less than about 3.5, and 3.5 which is above this range.

Table 6							
Example	Filler	Filler Size (μm)	Vol. % CaCO ₃	Izod (ft-lb/in)		Izod (J/m)	
				Near End	Far End	Near End	Far End
Comp. Ex. 26	Control		0	0.75	0.78	39.75	41.34
Comp. Ex. 27	UPF*	0.07	5	0.51	0.59	27.03	31.27
Comp. Ex. 28	UPF	0.07	15	0.54	0.4	28.62	21.2
Comp. Ex. 29	UPF	0.07	25	0.48	0.35	25.44	18.55
Ex. 15	S200	0.7	5	0.7	0.78	37.1	41.34
Ex. 16	S200	0.7	10	0.94	1.21	49.82	64.13
Ex. 17	S200	0.7	15	1.1	1.21	58.3	64.13

Example	Filler	Filler Size (μm)	Vol. % CaCO_3	Izod (ft-lb/in)		Izod (J/m)	
				Near End	Far End	Near End	Far End
Ex. 18	S200	0.7	20	1.13	1.26	59.89	66.78
Ex. 19	S200	0.7	25	1.07	1.05	56.71	55.65
Comp. Ex. 30	HPF**	3.5	5	0.78	0.67	41.34	35.51
Comp. Ex. 31	HPF	3.5	15	0.73	0.75	38.69	39.75
Comp. Ex. 32	HPF	3.5	25	0.78	0.73	41.34	38.69
*UPF is Ultra-Pflex [®]							
**HPF is HiPflex [®]							

EXAMPLES 20-25

- Following the procedure of Examples 3-5, two grades of 0.7-1 μm Magnifin[®] fatty acid coated magnesium hydroxide (Lonza, Inc, Fairlawn, NJ) were combined with Capron 8200 nylon 6. Results are shown in Table 7.

Table 7						
Properties of MgOH-filled nylon 6						
Example	Filler	Vol-% filler	Izod Impact (ft-lbs/in)		Izod Impact (J/m)	
			Near End	Far End	Near End	Far End
Comp. Ex. 33	Control	0	1.04	1.2	55.12	63.6
Ex. 20	Magnifin H-10C	5	1.41	1.41	74.73	74.73
Ex. 21	Magnifin H-10C	15	1.04	1.06	55.12	56.18
Ex. 22	Magnifin H-10C	25	1.04	0.96	55.12	50.88
Ex. 23	Magnifin H-5IV	5	0.96	1.28	50.88	67.84
Ex. 24	Magnifin H-5IV	15	0.96	1.2	50.88	63.6
Ex. 25	Magnifin H-5IV	25	0.96	0.96	50.88	50.88

EXAMPLES 26 AND 27, COMPARATIVE EXAMPLES 34 AND 35

- In Comparative Examples 34 and 35, Zytel[®] 101 and Zytel[®] 132F were each combined with Zytel[®] 70G643L 43% glass fiber filled nylon 66 in the feed hopper of the injection molding machine. The weight ratio was 1 part Zytel[®] 70G643L to 9 parts of the resin blend, to give 4.3 wt. % glass compositions. In Examples 26 and 27, the Zytel[®] resins were first extrusion blended with 20 vol % Super-Pflex[®] 0.7 μm stearic acid treated CaCO_3 , the thus blended resin then was mixed as in Comparative Examples 34 and 35. Test bars

were molded with a barrel temperature of 270°C and a mold temperature of 90°C. The data in Table 8 shows that in the presence of glass there is an improvement in izod toughness due to the addition of filler.

Table 8						
Properties of CaCO ₃ -Glass Filled Nylon 66						
			Izod Impact (ft-lb/in)		Izod Impact (J/m)	
Example	Resin	Vol% Filler	Near Izod	Far Izod	Near Izod	Far Izod
Comp. Ex. 34	Zytel® 101	0	0.62	0.7	32.86	37.1
Example 26	Zytel® 101	20	0.78	0.91	41.34	48.23
Comp. Ex. 35	Zytel® 132F	0	0.7	0.65	37.1	34.45
Example 27	Zytel® 132F	20	0.75	0.89	39.75	47.17

5

EXAMPLES 28-30 AND COMPARATIVE EXAMPLE 36

In Comparative Example 36, Zytel® 101 (DuPont) nylon 66 was melt-blended at 270°C with Capron® 8200 (Allied-Signal) nylon 6 in a 30/70 weight ratio. In Examples 28-30, Super-Pflex® 200 stearic-acid-coated calcium carbonate at 5, 10, and 20 vol. % was melt-blended with the Zytel® 101/Capron® 8200 30/70blend. All were subsequently molded into test bars. The test results are provided in Table 9. The results show an increase in Izod toughness in blends of nylon 6 and 66.

10

Table 9						
			Izod Impact (ft-lb/in)		Izod Impact (J/m)	
	E91653-125-	Vol-% Superpflex® 200	Near End	Far End	Near End	Far End
Comp. Ex 36	8	0	1.26	1.34	66.78	71.02
Ex. 28	9	5	0.88	1.04	46.64	55.12
Ex. 29	10	10	0.82	0.72	43.46	38.16
Ex. 30	11	20	1.53	1.55	81.09	82.15

15

EXAMPLES 31-33 AND COMPARATIVE EXAMPLE 37

In Comparative Example 37, Capron® 8200 nylon 6 was melt-blended with 20 vol. % of uncoated 0.7 µm Albafil® calcium carbonate. In Example 31, 1500 grams of uncoated Albafil® was mixed for 10 minutes in a V-cone blender with a solution of 15 grams of decanoic acid in 50 ml of chloroform. In Example 32, 1000 grams of uncoated Albafil® was mixed for 15 minutes in a V-cone blender with 20 grams of decanoic acid. In Example 33, 1000 grams of uncoated Albafil® was mixed for 15 minutes in a V-cone blender with 40 grams

20

of decanoic acid. All coated particles were dried overnight in a hood and then in an oven at 100°C for 1 hour. Both the uncoated and coated particles were melt-blended with Capron® 8200 nylon 6 to give a concentration of 20 vol. % and injection molded into bars. Table 10 shows that another saturated carboxylic acid, decanoic acid provides increased Izod toughness.

Table 10						
			Izod Impact (ft-lb/in)		Izod Impact (J/m)	
	E91653-	Wt% Decanoic Acid on Albafil® Filler	Near End	Far End	Near End	Far End
Comp. Ex. 37	142-2	0	0.62	0.81	32.86	42.93
Ex. 31	125-3	1	0.55	0.66	29.15	34.98
Ex. 32	148-6	2	0.6	0.63	31.8	33.39
Ex. 33	148-7	4	1.57	1.27	83.21	67.31

EXAMPLES 34-37 AND COMPARATIVE EXAMPLE 37

In Comparative Example 37, Capron® 8200 nylon 6 was melt-blended with 20 vol. % of uncoated 0.7 µm Albafil® calcium carbonate. In Example 34, 1500 grams of uncoated Albafil® was mixed for 10 minutes in a V-cone blender with a solution of 15 grams of stearic acid in 50 ml of chloroform. The coated particles were dried overnight in a hood. In Example 35, 1000 grams of uncoated Albafil® was mixed for 15 minutes in a V-cone blender with 20 grams of stearic acid in 100 ml of warmed chloroform. The coated particles were dried overnight in a hood and then in an oven at 100°C for 1 hour. In Example 36, 1500 grams of uncoated Albafil® was mixed for 10 minutes in a V-cone blender with a solution of 37.5 grams of stearic acid in 50 ml of chloroform. The coated particles were dried in an oven at 100°C for 1 hour. In Example 37, 1000 grams of uncoated Albafil® was mixed for 15 minutes in a V-cone blender with 40 grams of stearic acid in 150 ml of warmed chloroform. The coated particles were dried overnight in a hood and then in an oven at 100°C for 1 hour. Both the uncoated and coated particles were melt-blended with Capron® 8200 nylon 6 to give a concentration of 20 vol. % and injection molded into bars. Table 11 shows that a stearic acid concentration of about 2% on the particles was necessary to increase Izod toughness at 20 vol. % total filler. Table 11 also shows that pure stearic increased Izod toughness.

Table 11						
			Izod Impact (ft-lb/in)		Izod Impact (J/m)	
		Wt. % Stearic Acid on Albafil® Filler	Near End	Far End	Near End	Far End
Comp. Ex. 37	E91653-142-2	0.00	0.62	0.81	32.86	42.93
Ex. 34	E91653-125-5	1.00	0.53	0.58	28.09	30.74
Ex. 35	E94220-14-3	2.00	1.89	2.35	100.17	124.55
Ex. 36	E91653-142-7	2.50	2.21	2.37	117.13	125.61
Ex. 37	E94220-14-4	4.00	2.08	2.16		

EXAMPLES 38-40 AND COMPARATIVE EXAMPLE 37

- In Comparative Example 37, Capron® 8200 nylon 6 was melt-blended with 20 vol. % of uncoated 0.7 µm Albafil® calcium carbonate. In Example 38,
- 5 1500 grams of uncoated Albafil® was mixed for 10 minutes in a V-cone blender with a solution of 15 grams of zinc stearate in 30 ml of toluene. The coated particles were dried in an oven at 100°C for one hour. In Example 39, 1000 grams of uncoated Albafil® was mixed for 15 minutes in a V-cone blender with a
- 10 solution of 20 grams of zinc stearate in 100 ml of chloroform. In Example 40, 1000 grams of uncoated Albafil® was mixed for 15 minutes in a V-cone blender with a solution of 40 grams of zinc stearate in 150 ml of chloroform. The coated particles in Examples 39 and 40 were dried overnight in a hood and then in an oven at 100°C for one hour. Both the uncoated and coated particles were melt-
- 15 blended with Capron® 8200 nylon 6 to give a concentration of 20 vol. % and injection molded into bars. Table 12 shows that the zinc stearate salt increased Izod toughness.

Table 12						
			Izod Impact (ft-lb/in)		Izod Impact (J/m)	
	E91653-	Wt. % Zinc Stearate on Albafil® Filler	Near End	Far End	Near End	Far End
Comp. Ex. 37	142-2	0	0.62	0.81	32.86	42.93
Ex. 38	142-8	1	2.07	2.4	109.71	127.2
Ex. 39	148-10	2	1.54	1.49	81.62	78.97
Ex. 40	148-11	4	2	2.1	106	111.3

It is claimed:

1. A composition comprising nylon 6, nylon 66, or a mixture thereof, with about 1%-50% by volume of a mineral filler having an aspect ratio of less than about 5, the filler having an average equivalent spherical diameter in the range of about 0.1 to less than about 3.5 micrometers, and a saturated organic acid, a salt thereof, or a mixture thereof, at a concentration of at least 0.5% by weight of the mineral filler.
2. The composition according to Claim 1 wherein the composition comprises about 5-30% by volume of a mineral filler.
3. The composition according to Claim 1 wherein the composition comprises about 10-20% by volume of a mineral filler.
4. The composition of according to Claim 1 wherein the average equivalent spherical diameter is about 0.5 to about 2 micrometers.
5. The composition according to Claim 1 wherein the concentration of saturated organic acid, salt thereof, or mixture thereof is in the range of about 0.5-4%.
6. The composition according to Claim 1 wherein the saturated organic acid, salt thereof, or mixture thereof comprises one or more saturated fatty acids, salts thereof, or a mixture thereof.
7. The composition according to Claim 6 wherein the saturated fatty acid is stearic acid.
8. The composition according to Claim 4 wherein the saturated organic acid is stearic acid at a concentration of about 2% by weight on the weight of the filler.
9. The composition according to Claim 1 wherein the inorganic filler is calcium carbonate or titanium dioxide.
10. The composition according to Claim 1 comprising a shaped article.
11. A process for forming a composition comprising the steps of:
 - (a) combining nylon 6, nylon 66, or a mixture thereof with a mineral filler having an aspect ratio of less than 5, the filler having an average equivalent spherical diameter in the range of about 0.1 to less than about 3.5 micrometers, and a saturated organic acid, salt thereof, or mixture thereof, at a concentration of at least about 0.5% by weight of the mineral filler, the filler and polymer being combined at a weight ratio given by the formula:

$$W_f/W_p = [VF/(1-VF)] \cdot D_f/D_p$$

where W_f is the weight of the filler, W_p is the weight of the polymer, VF is the desired volume fraction of filler, in the range of about 0.01-0.5, D_f is the density of the filler, and D_p is the density of the polymer;

- 5 (b) heating the combination to a temperature above the melting point of the nylon to form a molten composition;
- (c) mixing the molten composition to provide a homogenous melt; and,
- (d) cooling the molten composition.

10 12. The process of Claim 11 wherein VF is in the range of about 0.10-0.20.

 13. The process of Claim 11 wherein the average equivalent spherical diameter is about 0.5-2 micrometers.

15 14. The process of Claim 11 wherein the saturated organic acid, salt thereof, or mixture thereof comprises saturated fatty acids, salts thereof, or a mixture thereof.

 15. The process of Claim 13 wherein the saturated organic acid is stearic acid at a concentration of about 2% by weight on the weight of the filler.

 16. The process of Claim 14 wherein the saturated fatty is stearic acid.

20 17. The process of Claim 11 wherein the inorganic filler is calcium carbonate or titanium dioxide.

DECLARATION and POWER OF ATTORNEY

As a below-named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

TOUGHENED, HIGH-MODULUS POLYAMIDES

the specification of which is attached hereto unless the following box is checked:

☒ was filed on **18 FEBRUARY 2000** as U.S. Application No. _____ or PCT International Application No. **PCT/US00/04105** and was amended on _____ (if applicable).

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is known to me to be material to patentability as defined in 37 CFR § 1.56.

I hereby claim foreign priority benefits under 35 U.S.C. § 119(a)-(d) or § 365(b) of any foreign application(s) for patent or inventor's certificate, or § 365(a) of any PCT International application which designated at least one country other than the United States, listed below and have also identified below, by checking the box, any foreign application for patent or inventor's certificate, or PCT International application having a filing date before that of the application on which priority is claimed.

Application No.	Country	Filing Date	Priority Claimed (Yes/No)
-----------------	---------	-------------	---------------------------

I hereby claim the benefit under 35 U.S.C. § 119(e) of any United States Provisional Application(s) listed below.

U.S. Provisional Application No.

60/120,671

U.S. Filing Date

19 FEBRUARY 1999

I hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s), or § 365(c) of any PCT International Application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application or PCT International Application in the manner provided by the first paragraph of 35 U.S.C. § 112, I acknowledge the duty to disclose information which is known to me to be material to patentability as defined in 37 CFR § 1.56 which became available between the filing date of the prior application and the national or PCT International filing date of this application.

Application No.	Filing Date	Status (patented, pending or abandoned)
-----------------	-------------	---

POWER OF ATTORNEY: I hereby appoint the following attorney(s) and/or agent(s) the power to prosecute this application and transact all business in the Patent and Trademark Office connected therewith:Name: **WILLIAM J. COTREAU**Registration No.: **36,4090**

Send correspondence and direct telephone calls to:

WILLIAM J. COTREAU**E. I. du Pont de Nemours and Company
Legal - Patents
Wilmington, DE 19898, U.S.A.****Tel. No.
(302) 992-4930
Fax No.
(302) 773-0164**

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

INVENTOR(S)

Full Name of Inventor	Last Name	First Name	Middle Name
	WEINBERG	MARK	
	Signature (please sign full name): <i>Mark Weinberg</i>		Date: <i>4/17/00</i>
Residence & Citizenship	City WILMINGTON	State or Foreign Country DELAWARE DE	Country of Citizenship U.S.A.
Post Office Address	Post Office Address 5 CHAPELCREST LANE	City WILMINGTON	State or Country DELAWARE
			Zip Code 19810

☐ Additional Inventors are being named on separately numbered sheets attached hereto.

GENERAL POWER OF ATTORNEY
(Concerning Several International Patent Applications)

The undersigned, Vernon R. Rice, Vice President and Assistant General Counsel of E. I. DU PONT DE NEMOURS AND COMPANY, 1007 Market Street, Wilmington, Delaware 19898 USA ("DuPont"), hereby confirms that the power to sign for DuPont has been granted to various individuals (as set forth in the attached excerpt from DuPont's Patent Board Rules of Procedure (January 1988), Appendix Section III.A.4), including the Chairman, Vice-Chairman, and those individuals who are Assistant Secretaries of the Patent Board. Currently these Assistant Secretaries are:

Roger A. Bowman
Linda J. Davis
John E. Griffiths

Barbara J. Massie
Miriam D. Meconnahey
Deborah A. Meginniss

In addition, the authority to act on behalf of DuPont before the competent International Authorities in connection with any and all international patent applications filed by it with the United States as Receiving Office and to make or receive payments on its behalf is hereby granted to:

Beardell, Lori Y.	34,293	Kuller, Mark D.	31,925
Belopolsky, Inna	43,319	Krukiel, Charles E.	27,344
Benjamin, Steven C.	36,087	Jarnholm, Arne R.	30,396
Birch, Linda D.	38,719	Langworthy, John A.	32,255
Bowen, Jr., Alanson G.	24,027	Lerman, Bart E.	31,897
Christenbury, Lynne M.	30,971	Levitt, Cary A.	31,848
Cotreau, William J.	36,490	Li, Kening	44,872
Deitch, Gerald E.	30,457	Magee, Thomas H.	27,355
Deshmukh, Sudhir	33,677	Mayer, Nancy S.	29,190
Dobson, Kevin S.	40,296	Medwick, George M.	27,456
Duffy, Roseanne R.	33,869	Morrissey, Bruce W.	30,663
Edwards, Mark A.	39,542	Reynolds, Stephen E.	37,580
Estrin, Barry	26,452	Rizzo, Thomas M.	41,272
Evans, Craig H.	31,825	Santopietro, Lois A.	36,264
Fair, Tamera L.	35,867	Schaeffer, Andrew L.	33,605
Feltham, S. Neil	36,506	Sebree, Chyrrea J.	45,348
Floyd, Linda Axiemethy	33,692	Shafer, Robert J.	24,437
Frank, George A.	27,636	Shay, Lucas K.	34,724
Golian, Andrew G.	25,293	Shipley, James E.	32,003
Gorman, Thomas W.	31,959	Siegeff, Barbara C.	30,684
Gould, David J.	25,338	Sinnott, Jessica M.	34,015
Griffiths, John E.	32,647	Steinberg, Michael A.	43,160
Hamby, Jane O.	32,872	Steinberg, Thomas W.	37,013
Hamby, William H.	31,521	Stevenson, Robert B.	26,039
Heiser, David E.	31,366	Strickland, Frederick D.	39,041
Hendrickson, John S.	30,847	Tessari, Joseph A.	32,177
Joung, J. Kenneth	41,881	Tulloch, Rebecca W.	36,297
Katz, Elliott A.	26,396	Walker, P. Michael	32,602
Kelly, Patricia L.	39,247	Wang, Chen	38,650
King, Karen K.	34,850		

The undersigned ratifies fully all actions already taken by the above-named individuals in accordance with the authority granted hereby.

E. I. DU PONT DE NEMOURS AND COMPANY

By: 

Vernon R. Rice

Vice President and Assistant General Counsel

Date: 9-13-00